

Removal of Hydrogen Sulfide from Groundwater by Granular Activated Carbon

Keisuke Ikehata, PhD, PE, PEng

Pacific Advanced Civil Engineering (PACE), Inc.

Fountain Valley, CA



Co-authors and Acknowledgements

▶ Co-authors

- ▶ Andrew T. Komor, Yuan (Abby) Li, Xiaoyan (Leo) Ou - PACE
- ▶ Jay A. Kleinheinz, Duncan S. Lee - City of Huntington Beach
- ▶ C. Bryan Trussell, David R. Hokanson - Trussell Technologies



▶ Acknowledgements

- ▶ Steve Styles, Chris Cassotta, Derek Smith - City of Huntington Beach

Introduction

- ▶ Project locations: City of Huntington Beach's three potable wells
 - ▶ Well 3
 - ▶ Well 6
 - ▶ Well 9
- ▶ Design Capacity: 3,000 to 3,500 GPM each
- ▶ Current treatment
 - ▶ Chlorination (Free Cl_2 with gaseous Cl_2)
 - ▶ Fluoridation (HF)



Project Objective

- ▶ Utilize the groundwater to maximize the local water resources in the current drought situations
 - ▶ Historically the wells haven't been run at their full speed (50% to 60%)
 - ▶ Water quality concerns at the design production rates
 - ▶ Color (NOM): <5 CU → up to 15 CU
 - ▶ H₂S: non-detect → up to 0.2 mg/L
 - ▶ Addition of treatment facilities has been considered
 - ▶ Granular activated carbon (GAC)
 - ▶ Chlorine-bisulfite-chlorine
 - ▶ Ozone
 - ▶ GAC-based treatment has already been selected for one of the wells
 - ▶ Being considered at the other wells

Pilot Study Objectives

- ▶ GAC-based treatment has been tested by the City of Huntington Beach and a full-scale demo filter has been installed and used at Well 9 since 2010
 - ▶ The demo filter has a design capacity of 250 gpm
 - ▶ Coconut shell-based media
 - ▶ No backwash
- ▶ A series of pilot studies have been carried out
 - ▶ To evaluate the feasibility of the GAC-based treatment
 - ▶ To identify H₂S removal mechanisms
 - ▶ To ensure no odor or other unexpected water quality issues in the distribution system
 - ▶ To determine full-scale design parameters



History of On-site Pilot Studies

- ▶ 2006: Initial pilot study (up to 30 gpm) at Well 9
- ▶ 2009: Demo GAC filter vessel (250 gpm, sidestream) at Well 9
- ▶ 2014: Demo GAC filter monitoring (with chlorine) at Well 9 (Up to 350 gpm)
- ▶ 2014: Small pilot GAC at Well 9 (0.25 gpm)
- ▶ 2014: Demo GAC filter monitoring (without chlorine) at Well 9 (Up to 400 gpm)
- ▶ 2014-2015: Small pilot GAC at Wells 6 and 3 (Up to 0.6 gpm, reduced filter bed depth)
- ▶ 2015: Demo GAC filter monitoring (reduced filter bed depth) at Well 9 (ongoing)
- ▶ 2015: Small pilot GAC and non-GAC at Well 9 (Up to 0.6 gpm)

NOTE: Full-scale filters are being designed for Well 9

General Methodologies

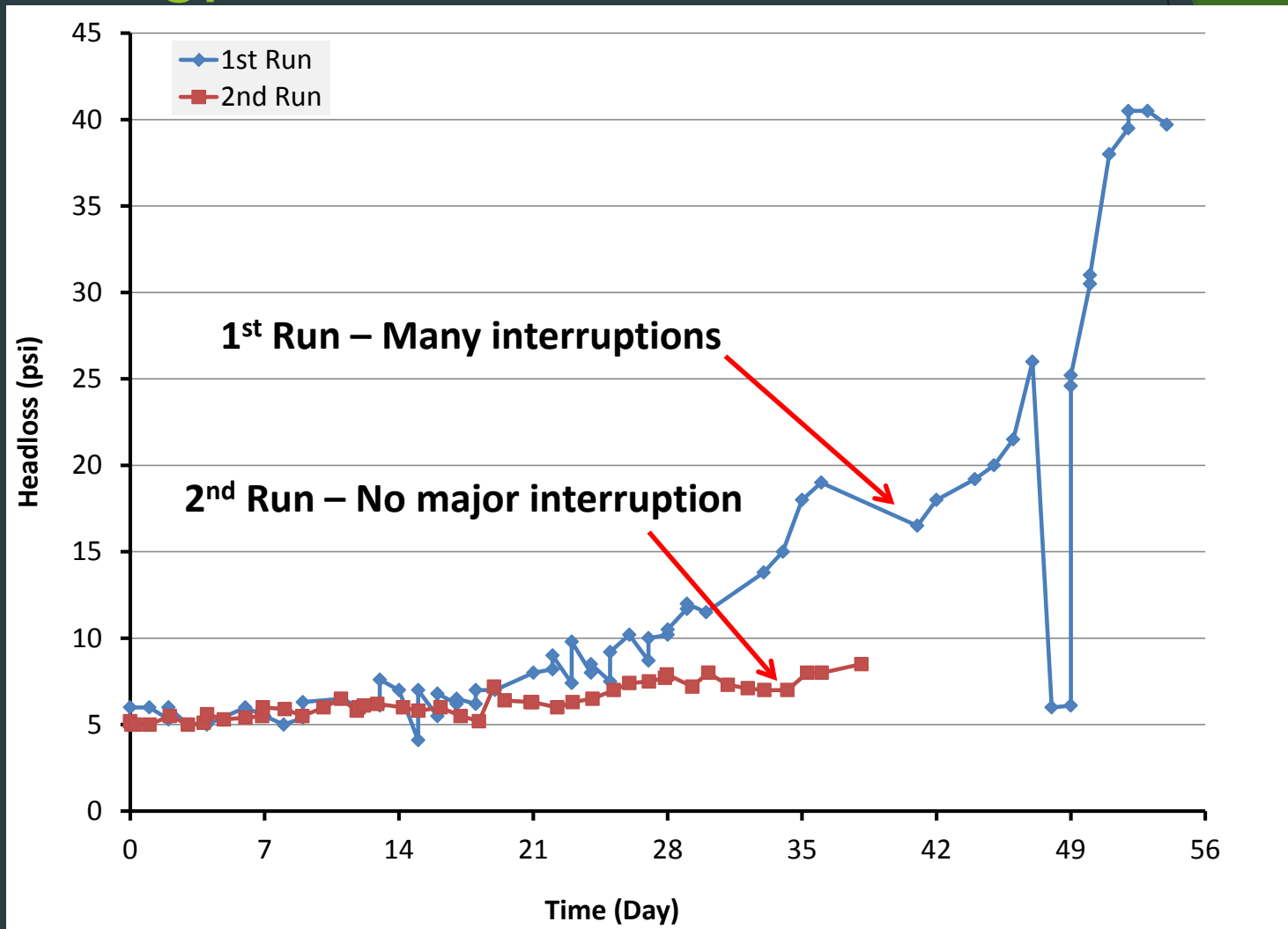
- ▶ Pilot filters: Two scales
 - ▶ Demo GAC filter at Well 9 (250 to 400 gpm)
 - ▶ 10' diameter
 - ▶ Surface loading rate: 3.5 to 5.6 gpm/ft²
 - ▶ Pilot filtration skid (0.25 to 0.6 gpm)
 - ▶ Five 2' filter columns (3" ID clear PVC), in series or in parallel
 - ▶ Surface loading rate: 5.1 to 12.8 gpm/ft²
 - ▶ GAC media and non-GAC media
- ▶ Study periods
 - ▶ 4 to 8 weeks each
- ▶ Water quality parameters monitored
 - ▶ H₂S, color
 - ▶ pH, DO, ORP, TDS, temperature, turbidity, nitrate, odor, HPC, TOC
 - ▶ A flow cell was used to measure DO and ORP accurately



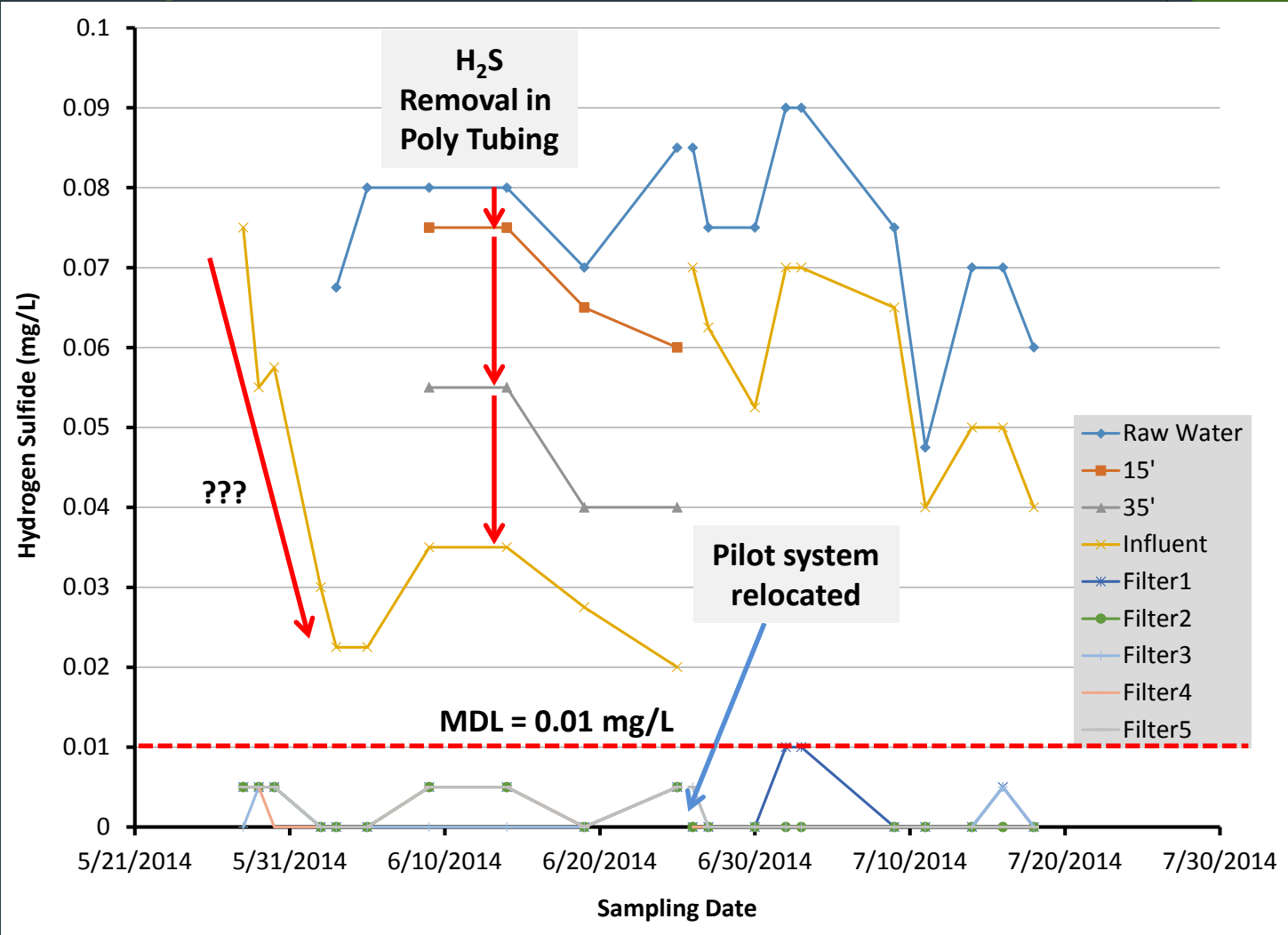
Coconut Shell GAC Media Specifications

- ▶ Mesh size: 12 x 30
- ▶ NSF 61 certified
- ▶ Carbon tetrachloride #: 60%
- ▶ Iodine #: 1,100 min
- ▶ Ash, weight %: 3 max
- ▶ Hardness %: 98 min
- ▶ Moisture as packed wt%: 3 max
- ▶ Apparent density g/cc: 0.45-0.52

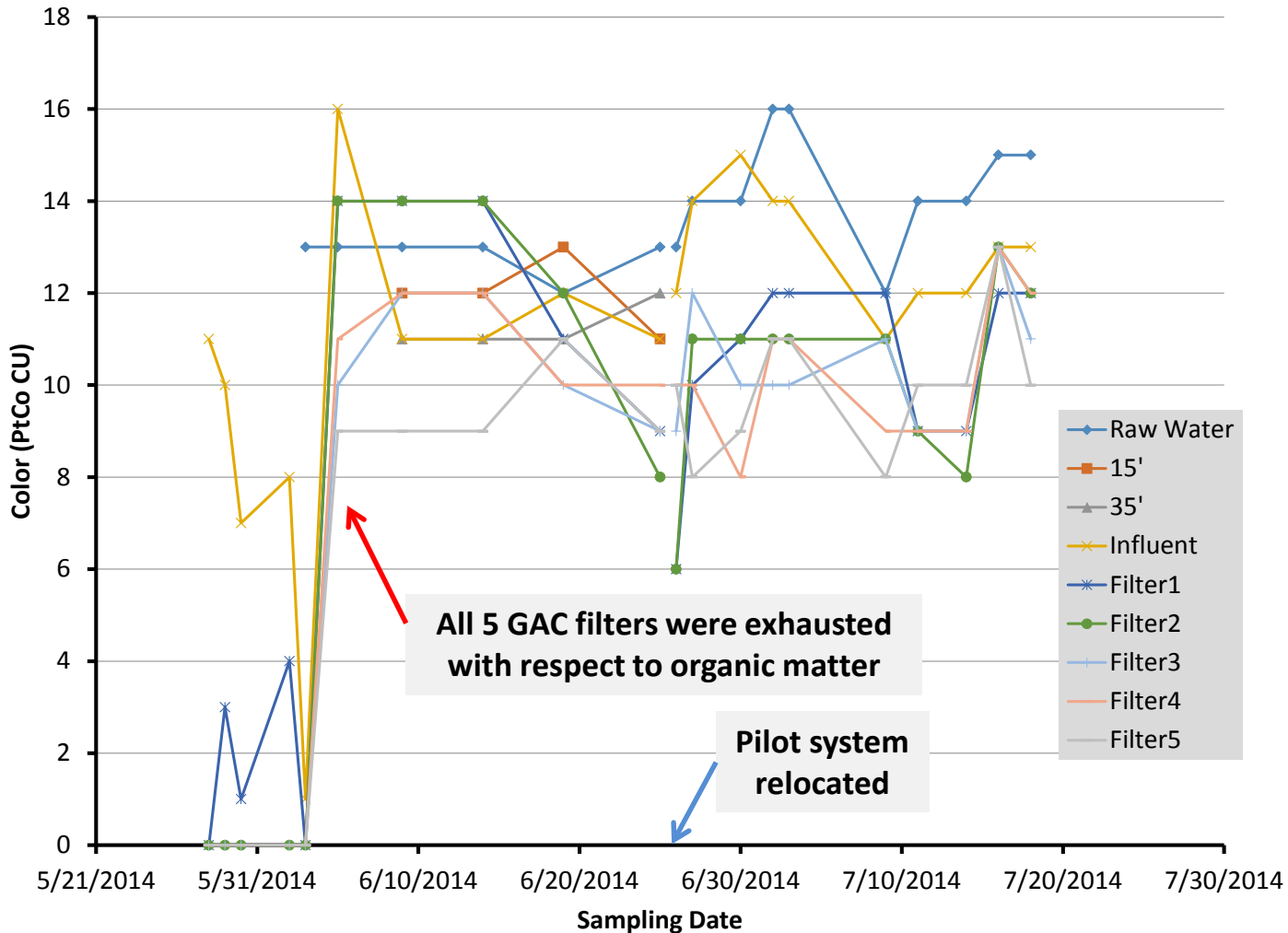
Head Loss in GAC Filters (0.25 gpm, 5 Filters in Series)



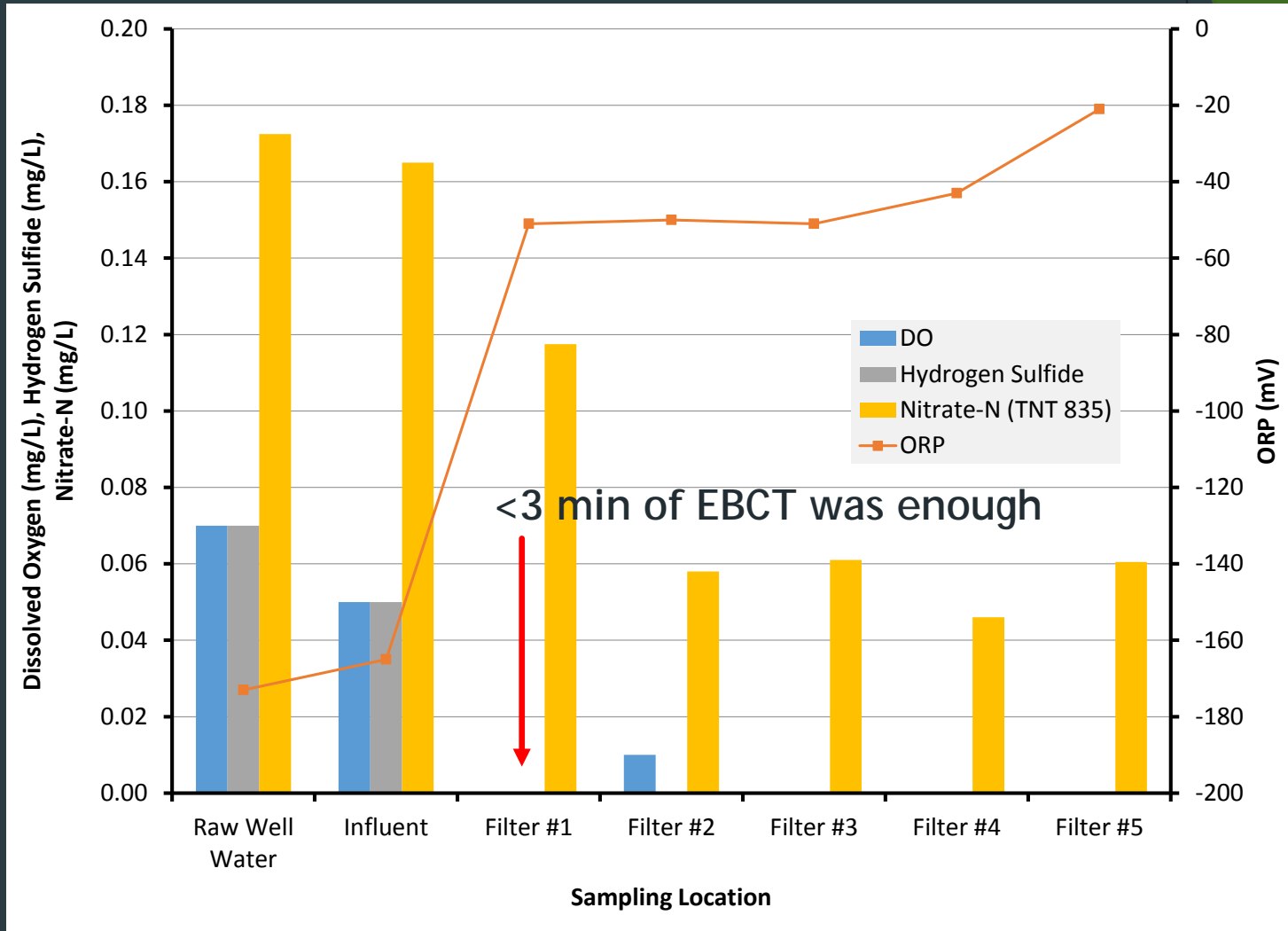
H₂S Removal in GAC Filters (0.25 gpm, 5 Filters in Series)



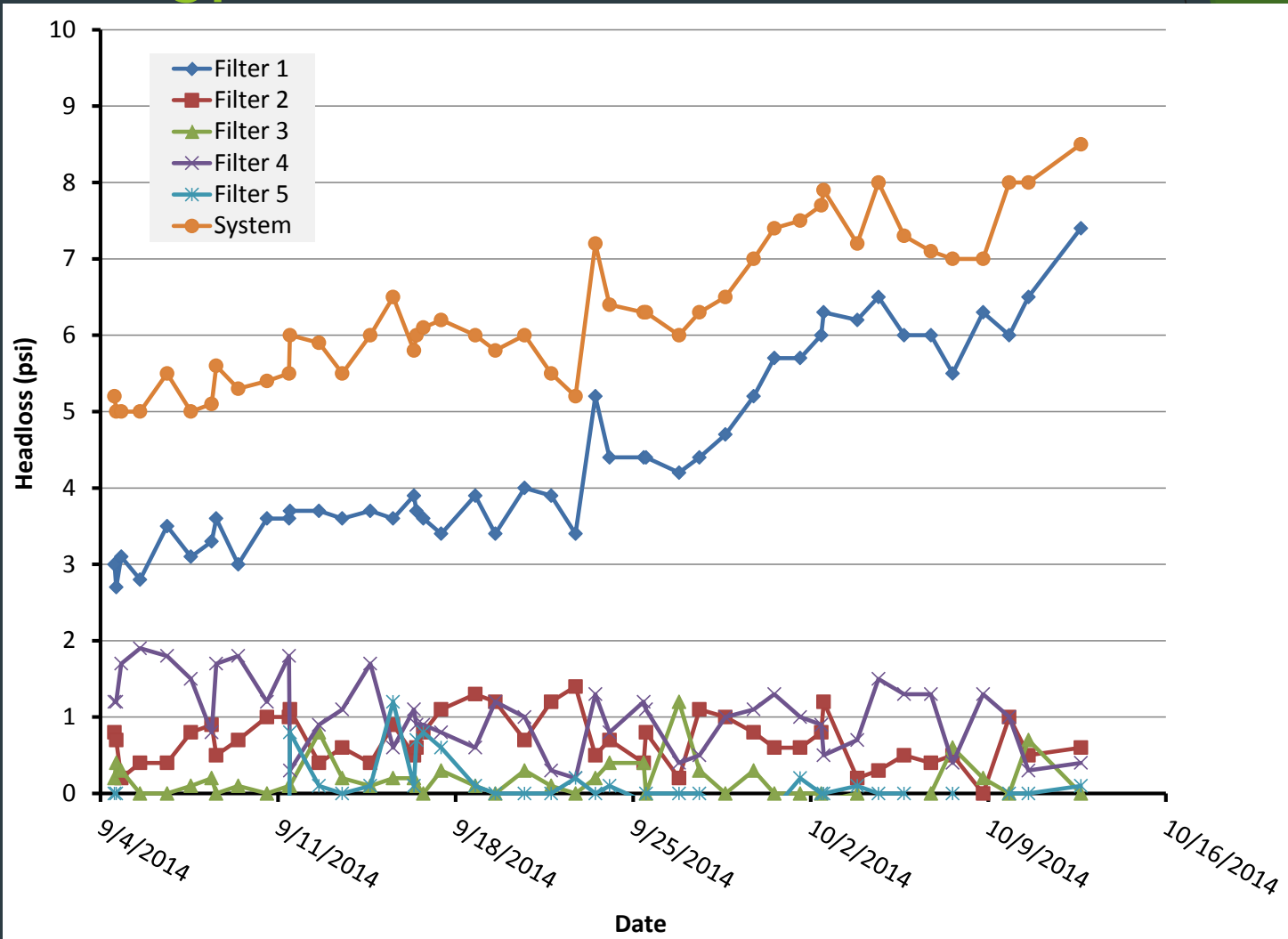
Color Removal in GAC Filters (0.25 gpm, 5 Filters in Series)



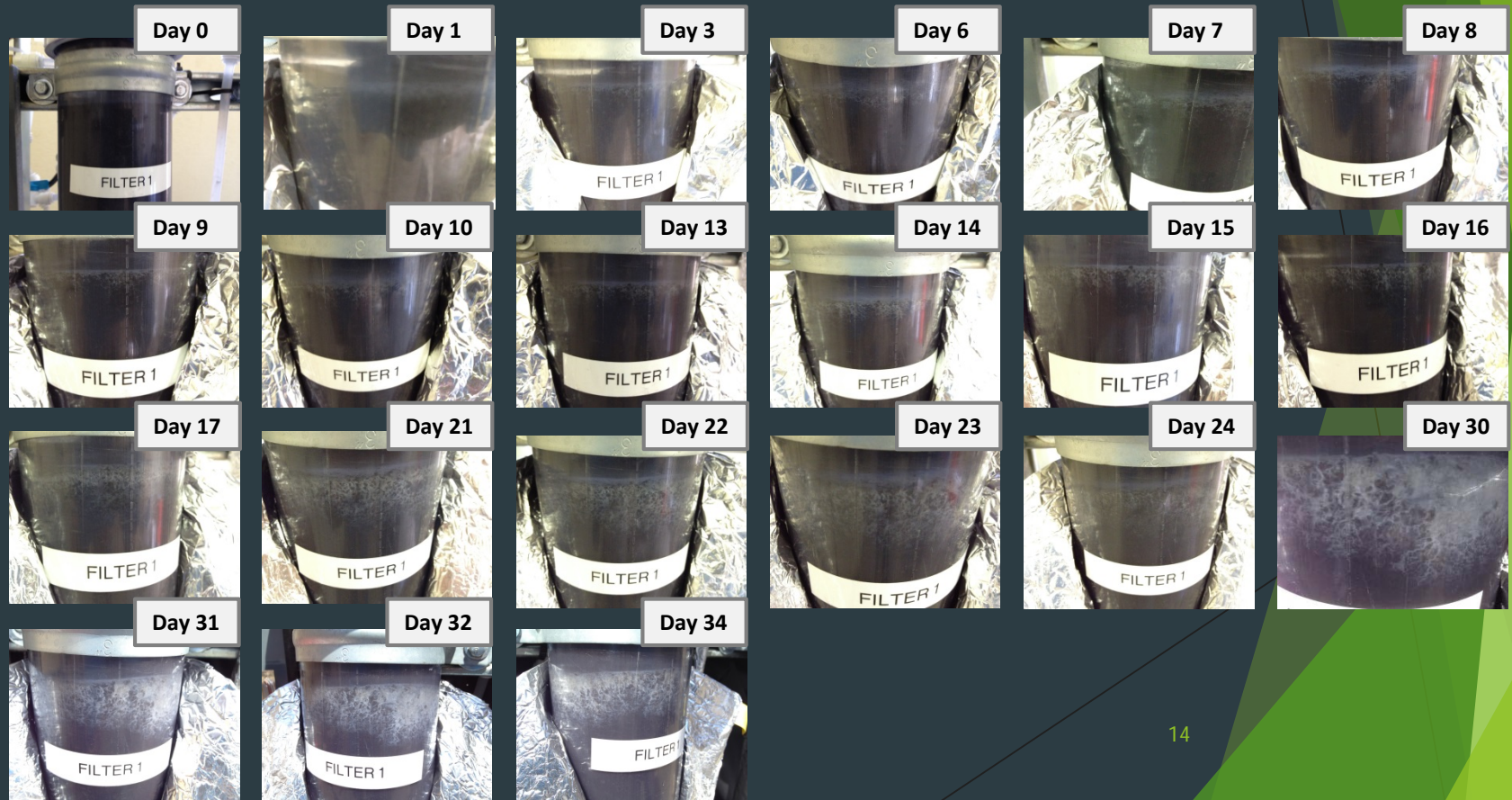
H₂S, DO, Nitrate-N, and ORP (0.25 gpm, 5 Filters in Series)



Head Loss in GAC Filters (0.25 gpm, 5 filters in Series)



Colonization at the Surface of Filter 1 (0.25 gpm, 5 Filters in Series)

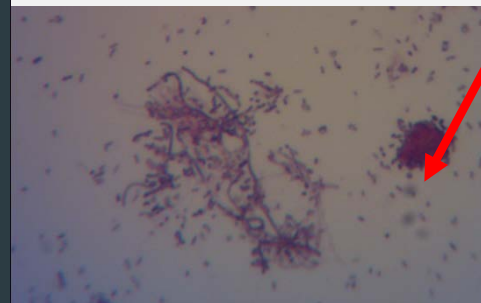


H₂S Removal Mechanisms

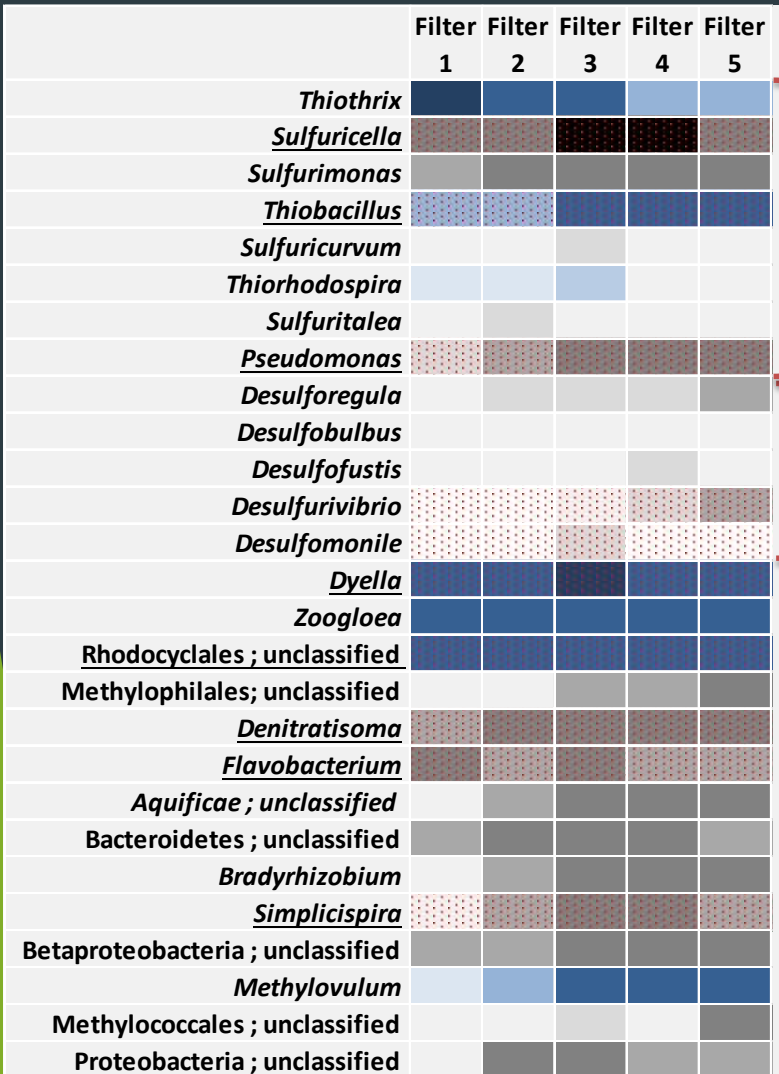
- ▶ Physicochemical
 - ▶ Adsorption/catalytic oxidation
 - ▶ Only at the start up (a few days)
 - ▶ Chlorine/Mn-mediated oxidation
 - ▶ No chlorine
- ▶ Biological
 - ▶ *Thiobacillus* spp.
 - ▶ Autotrophic denitrifier
 - ▶ *Thiothrix* spp.
 - ▶ Gram-negative, microaerobic sulfide oxidizer



Gram-negative, rod-shape cells forming filaments



16S rRNA Analysis



Sulfur Oxidizers

Sulfate Reducers

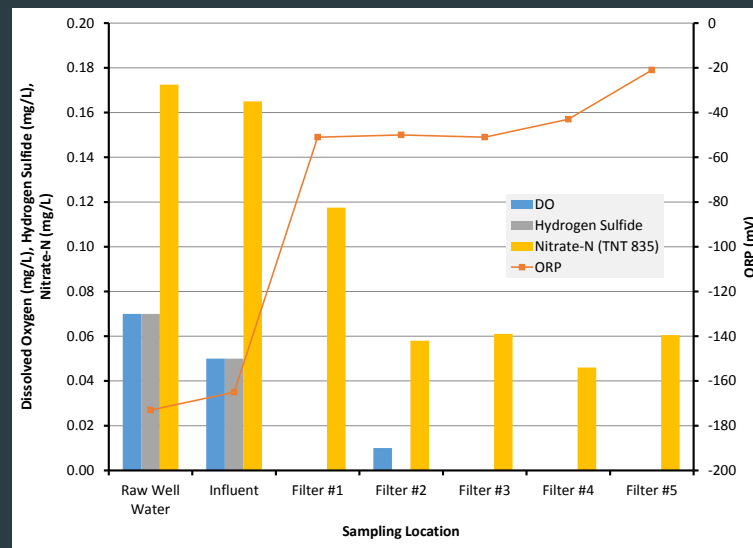
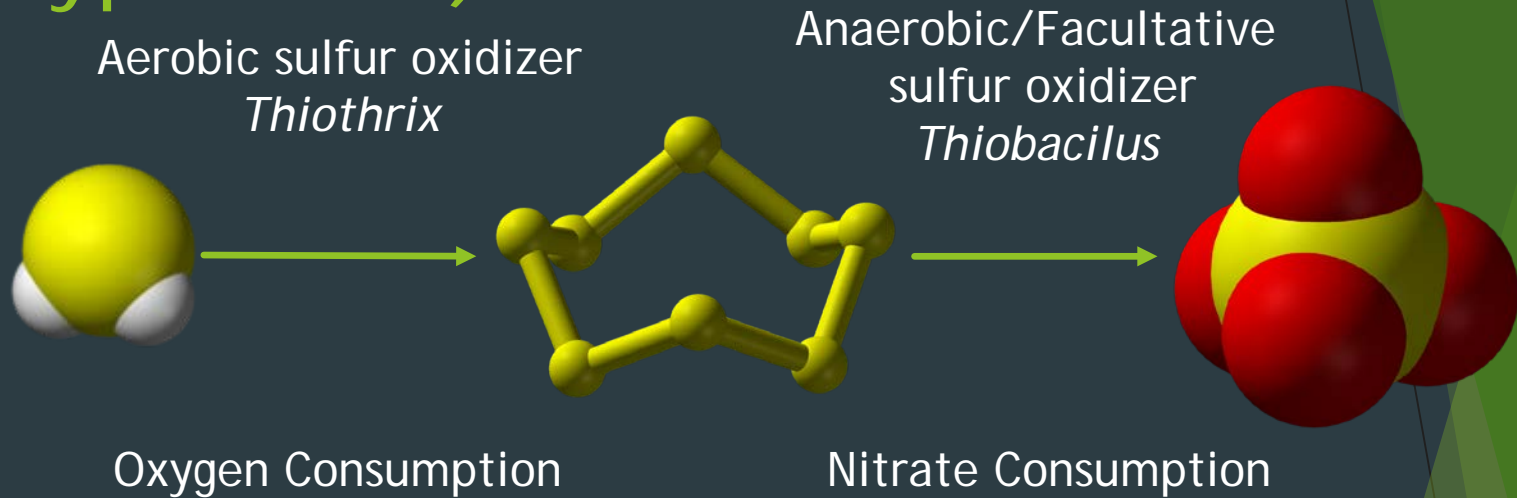


Denitrifying Bacteria (Certain species)

Quantity	Anaerobe/ Facultative anaerobe	Aerobe
0-10	Light Blue	Light Blue
10-100	Medium Blue	Medium Blue
100-1000	Dark Blue	Dark Blue
1000-10000	Very Dark Blue	Very Dark Blue
10000-30000	Black	Black

- Aerobic sulfur oxidizer in the top 2'
 - e.g., *Thiothrix*
- Anaerobic/facultative sulfur oxidizers in the middle
 - e.g., *Sulfuricella*, *Thiobacillus*
- Sulfate reducers at the bottom 2'
 - e.g., *Desulforegula*, *Desulfurivibrio*

Microbial Oxidation of H₂S (Hypothesis)



Byproducts and Odor

- ▶ Elemental sulfur
- ▶ Polysulfides
 - ▶ Products of elemental sulfur and H_2S
 - ▶ HS_nH
 - ▶ Matchstick odor
- ▶ Elemental sulfur was detected in the Demo GAC filter effluent
- ▶ Polysulfide was non-detect
 - ▶ However, a very slight matchstick odor was present in some of the filter effluent samples
 - ▶ Need more sensitive sulfur analysis methods

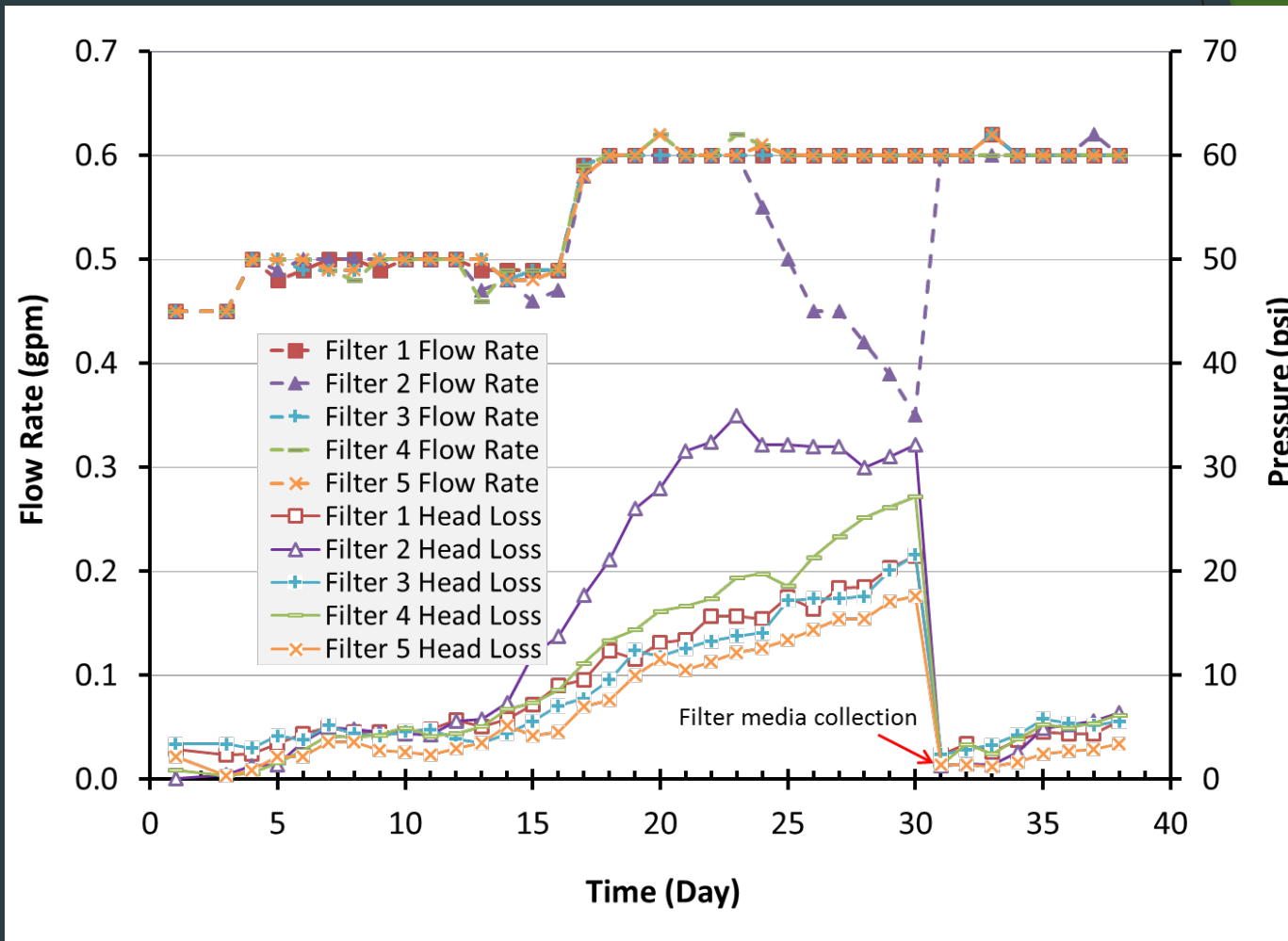
Odor Test GAC + Chlorination

Current

Future

Incubation Time	Raw	Chlorinated-Fluoridated Raw	GAC Treated	Chlorinated-Fluoridated GAC Treated
<30 min	Strong rotten egg	Strong smoky/match stick	No odor	Strong bleach
3 hours	Weak rotten egg	Strong smoky/match stick	No odor	Bleach
6 hours	No odor	Strong smoky/match stick	No odor	Bleach
Implications	Hydrogen sulfide was present, dissipated during the incubation	Polysulfide was present, very persisting odor	No hydrogen sulfide/ polysulfide was present	No hydrogen sulfide/ polysulfide was present

High Flow Rate, Short EBCT (12.8 gpm/ft², 1.2 min, Parallel)



Conclusions

- ▶ GAC-based H₂S removal is feasible, repeatable, consistent and almost instantaneous
 - ▶ Coconut-shell based GAC
 - ▶ Worked at all three well sites
- ▶ No odorous byproducts before/after chlorination
- ▶ The primary removal mechanism is microbial
 - ▶ DO, ORP and nitrate are important parameters to monitor
 - ▶ Sulfate reduction may occur if the EBCT is too long
- ▶ Service flow rate can be as high as 13 gpm/ft²
- ▶ EBCT can be as short as 1 min
 - ▶ Bed depth: Minimum 2'
 - ▶ Huge savings in capital and O&M costs
- ▶ The filters can be run for at least 3 to 4 weeks
 - ▶ Up to a few years (the demo filter at Well 9)
 - ▶ Backwash will remove excess biomass and elemental sulfur

THANKS

Contact Information:

Keisuke Ikehata, PhD, PE, PEng

(714) 481-0662

kikehata@pacewater.com